

1           **Characterizing the reactivity of metallic iron upon methylene blue**  
2                           **discoloration in Fe<sup>0</sup>/MnO<sub>2</sub>/H<sub>2</sub>O systems**

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6  
7    **Abstract**

8    A simple method is proposed for testing the reactivity of elemental iron materials (Fe<sup>0</sup>  
9    materials) using methylene blue (MB) as reagent. The method is based on the oxidative  
10   reactivity of Fe<sup>II</sup> for reductive dissolution of MnO<sub>2</sub>. Fe<sup>II</sup> is produced in-situ by the oxidation  
11   of a Fe<sup>0</sup> material. The in-situ formed Fe<sup>II</sup> reacted with MnO<sub>2</sub> delaying the bulk precipitation of  
12   iron corrosion products and thus MB co-precipitation (MB discoloration). For a given MnO<sub>2</sub>,  
13   the extent of MB discoloration delay is a characteristic of individual Fe<sup>0</sup> materials under given  
14   experimental conditions. The MB discoloration method for testing the reactivity of Fe<sup>0</sup>  
15   materials is facile, cost-effective and does not involve any stringent reaction conditions.

16   **Keywords:** Adsorption, Co-precipitation, Methylene blue, Manganese oxides, Reactivity,  
17   Zerovalent iron.

18   **Introduction**

19   Since the introduction of permeable reactive barriers of metallic iron for groundwater  
20   remediation (Fe<sup>0</sup> PRB technology), various Fe<sup>0</sup> types were tested and mostly successfully  
21   used for environmental remediation. Despite the reported successes, little progress has been  
22   made toward characterizing the variability in reactivity among Fe<sup>0</sup> samples from different  
23   sources [1,2]. Available works attempted to relate corrosion rates to: (i) the rate of hydrogen  
24   evolution [3,4] or (ii) to the extend of contaminant removal by used Fe<sup>0</sup> materials [1,5].  
25   Among the reactivity parameters, the composition of the aqueous solution, the Fe<sup>0</sup> elemental  
26   composition (alloying elements) and the surface properties (specific surface area, oxidation

27 state) have been largely discussed [3,6,7]. However, none of these parameters is independent  
28 and  $\text{Fe}^0$  aqueous reactivity further depends on method of manufacture [8,9]. According to Van  
29 Orden [8], whether a metal is cast, forged, wrought or welded are as important as the  
30 environment in the corrosion process. One major limitation of the current material testing  
31 procedures is that each material is used for remediation tests and the reactivity is ascertained  
32 at the end of the possibly cost-intensive and time consuming experiments. An alternative  
33 approach consisting in testing the reactivity of  $\text{Fe}^0$  materials in dilute EDTA  
34 (ethylenediaminetetraacetic acid) was recently presented [2]. However, EDTA is a strong  
35 chelating agent known to delay the process of iron hydroxide precipitation [10] at near neutral  
36 pH which is characteristic for most natural systems.

37 There is a need to develop simple, reliable and cost-effective methods to test the reactivity of  
38  $\text{Fe}^0$  materials. Ideally such methods should (i) be performed under conditions where iron  
39 solubility is not enhanced, and (ii) be applicable for material screening in preliminary works  
40 to avoid analytical cost. This study proposed a simple approach to compare the reactivity of  
41  $\text{Fe}^0$  toward methylene blue discoloration. Four materials of known relative reactivity [2] were  
42 tested to ascertain the efficiency of the new method. The selected materials are representative  
43 for the large array of powdered and granular  $\text{Fe}^0$  materials used in environmental remediation.

#### 44 **Background of the experimental methodology**

45 Methylene blue (MB) discoloration in the presence of  $\text{Fe}^0$  results mostly from MB co-  
46 precipitation with in situ generated iron corrosion products [11,12]. Therefore, in a  $\text{Fe}^0/\text{H}_2\text{O}$   
47 system, the extend of MB discoloration should increase steadily from the start of the  
48 experiment to the time of total discoloration. If the process of corrosion product precipitation  
49 is delayed, the resulting MB discoloration is also delayed.

50 The differentiation of the reactivity of  $\text{Fe}^0$  materials in  $\text{Fe}^0/\text{MB}/\text{H}_2\text{O}$  systems is based on the  
51 reaction of  $\text{Fe}^{\text{II}}$  with  $\text{MnO}_2$  [13,14].  $\text{Fe}^{\text{II}}$  is generated in-situ from  $\text{Fe}^0$  oxidation. Because  
52 liberated  $\text{Fe}^{\text{II}}$  species are used for the reductive dissolution of  $\text{MnO}_2$  (at the  $\text{MnO}_2$  surface),

53 they are not available for quantitative MB co-precipitation. Thus, the blue intensity of MB  
54 solution will not decreased as rapidly as in the system without MnO<sub>2</sub>. Accordingly, for  
55 parallel experiments with a given MnO<sub>2</sub> and various Fe<sup>0</sup> samples, the extent of MB  
56 discoloration will be a reflection of the chemical reactivity of individual Fe<sup>0</sup> samples.  
57 Therefore, if a Fe<sup>0</sup> sample is low reactive no or little delay of MB discoloration will be  
58 observed (**assumption 1**). For reactive Fe<sup>0</sup> samples the more reactive the sample the more  
59 extensive the discoloration delay (**assumption 2**).

60 The used methodology for testing the reactivity of Fe<sup>0</sup> in MnO<sub>2</sub>/MB/H<sub>2</sub>O systems consists in  
61 following the process of MB discoloration in a given MnO<sub>2</sub>/H<sub>2</sub>O system as influenced by  
62 various Fe<sup>0</sup> while testing the validity of assumptions 1 and 2. It should be kept in mind that  
63 MB discoloration and not MB removal is discussed in this study. For the discussion of MB  
64 removal TOC measurements for instance should have been necessary to account for MB  
65 reduction to colorless leuco-methylene blue (LMB) [15] which remains in solution.

## 66 **Materials and Methods**

### 67 **Solutions**

68 Methylene blue (MB) is a traditionally favourite dye of choice for laboratory and technical  
69 purposes [16,17]. Its molecule has a minimum diameter of approximately 0.9 nm [18] and is  
70 also used as redox indicator [15]. The used initial concentration was 12 mg/L (~0.037 mM)  
71 MB and it was prepared by diluting a 1000 mg/L stock solution. All chemicals were analytical  
72 grade.

### 73 **Solid materials**

74 One scrap iron (ZVI1) and three commercially available iron materials (ZVI2 to ZVI4) have  
75 been tested in the present study. Table 1 summarizes the main characteristics of these  
76 materials together with their iron content. Before used ZVI4 (Tab. 1) was crushed and sieved;  
77 the size fraction 1.0-2.0 mm was used without any further pretreatment. The specific surface  
78 area of the materials were not available nor determined. This parameter is known as one of the

79 most important reactivity factors [20]. However, it is not the objective of this study to  
80 investigated the impact of the specific surface area on the reactivity of the material, but rather  
81 to compare the material in the form in which they could be used in field applications.  
82 Therefore, all other materials were used as obtained. Crushing and sieving ZVI4 aimed at  
83 working with materials of particle size relevant for field applications. The materials differ  
84 regarding their characteristics such as content of metallic iron, additives, grain size and shape.  
85 No information about the manufacture process (e.g. raw material, heat treatment) was  
86 available.

87 The used  $\text{MnO}_2$  is commercial sample from Merck (85 - 90%  $\text{MnO}_2$ ; synthetic pyrolusite).  
88 The powdered sample was used without any pre-treatment.

### 89 **Discoloration studies**

90 Batch experiments with a shaking intensity of  $50 \text{ min}^{-1}$  were conducted in essay tubes for an  
91 experimental duration of 6 days. The essay tubes were immobilized on a support frame. A  
92 rotary shaker HS 501 D from “Janke & Kunkel”, DCM Laborservice was used. The batches  
93 consisted of 0 to 9.0 g/L of the synthetic pyrolusite ( $\text{MnO}_2$ ) and 5 g/L of each  $\text{Fe}^0$ . A parallel  
94 experiments with the  $\text{Fe}^0$  materials alone was performed. The extent of MB discoloration in  
95 the investigated systems was characterized by allowing 0.0 to 0.20 g of  $\text{MnO}_2$  and 0.11 g of  
96 each  $\text{Fe}^0$  to react in sealed sample tubes containing 22.0 mL of a MB solution (12 mg/L) at  
97 laboratory temperature (about  $20 \pm 2 \text{ }^\circ \text{C}$ ). Initial pH was  $\sim 7.8$ . After equilibration, up to 3 mL  
98 of the supernatant solutions were carefully retrieved (no filtration) for MB measurements (no  
99 dilution). Each experiment was performed in triplicate and averaged results are presented.

### 100 **Analytical methods**

101 MB concentrations were determined by a Cary 50 UV-Vis spectrophotometer at a wavelength  
102 of 664.5 nm using cuvettes with 1 cm light path. The pH value was measured by combined  
103 glass electrodes (WTW Co., Germany). Electrodes were calibrated with five standards

104 following a multi-point calibration protocol in agreement with the current IUPAC  
105 recommendation [21].

## 106 **Expression of experimental results**

107 After the determination of the residual MB concentration (C) the corresponding percent MB  
108 discoloration was calculated according to the following equation (Eq. 1):

$$109 \quad P = [1 - (C/C_0)] * 100\% \quad (1)$$

110 where  $C_0$  is the initial aqueous MB concentration (about 12 mg/L), while C gives the MB  
111 concentration after the experiment. The operational initial concentration ( $C_0$ ) for each case  
112 was acquired from a triplicate control experiment without additive material (so-called blank).  
113 This procedure was to account for experimental errors during dilution of the stock solution,  
114 MB adsorption onto the walls of the reaction vessels and all other possible side reaction  
115 during the experiments.

## 116 **Results and Discussion**

### 117 **Effect of $MnO_2$ on the process MB discoloration in $Fe^0/H_2O$ systems**

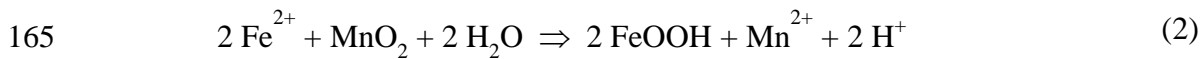
118 Figure 1 compares the extent of MB discoloration in the three investigated systems: (i) 0 to  
119 9.0 g/L  $MnO_2$  (System I), (ii) 0 to 9.0 g/L  $Fe^0$  (System II) and (iii) 5 g/L  $Fe^0$  and 0 to 9.0 g/L  
120  $MnO_2$  (System III). From Figure 1a it can be seen that System II is more efficient at  
121 discolouring MB at all tested material loadings. This observation is consistent with the  
122 intrinsic nature of both materials.  $MnO_2$  acts mostly as an absorbent with limited adsorption  
123 capacity.  $Fe^0$  and its oxidation products can adsorb MB. Oxidation products of  $Fe^0$  include  
124  $Fe(OH)_2$ ,  $Fe(OH)_3$ ,  $FeOOH$ ,  $Fe_2O_3$ ,  $Fe_3O_4$ , and green rust [22-24]. Their role in the  
125 mechanisms of aqueous contaminant removal is yet to be properly characterized [24,25]. It is  
126 certain that, during their precipitation corrosion products sequester MB in their structure  
127 [11]. Therefore, in a  $Fe^0/MB/H_2O$  system, MB discoloration may occur via adsorption and co-  
128 precipitation. Reduction to colourless LMB is also likely to occur. Whatever the actual MB  
129 discoloration mechanisms in  $Fe^0/H_2O$  systems are, the addition of various amounts of  $MnO_2$

130 to 5 g/L Fe<sup>0</sup> should have increased the extend of MB discoloration relative to the experiment  
131 with 5 g/L Fe<sup>0</sup> alone as represented in Fig. 1a. Accordingly, the discoloration extend of 52 %  
132 with 5 g/L Fe<sup>0</sup> in the absence of MnO<sub>2</sub> should increase with increasing MnO<sub>2</sub> loading to reach  
133 95 % discoloration at 9.0 g/L MnO<sub>2</sub>. This theoretical prediction (Fig. 1a) could not be verified  
134 experimentally as shown in Fig. 1b. Instead of increasing with increasing MnO<sub>2</sub> loading, the  
135 discoloration extent decreased from 52 % at 0 g/L MnO<sub>2</sub> to 40 % for MnO<sub>2</sub> loadings > 2 g/L.  
136 This observation is compatible with MB co-precipitation as main discoloration mechanism.  
137 The observed discoloration extent of 40 % for MnO<sub>2</sub> loadings > 2 g/L corresponds to the  
138 discoloration in: (i) system I (MnO<sub>2</sub> alone) for MnO<sub>2</sub> loadings > 6.5 g/L or (ii) system II (Fe<sup>0</sup>  
139 alone) for Fe<sup>0</sup> loadings > 2.0 g/L. This observation suggests that mixing 5 g/L Fe<sup>0</sup> with 0 to  
140 9.0 g/L MnO<sub>2</sub> results in a system less efficient at discolouring MB than a system with only  
141 2.5 g/L Fe<sup>0</sup>. Note that if MB was acting as redox indicator, the discoloration extend should  
142 have steadily increased with increasing MnO<sub>2</sub> loading. This observation corroborates the  
143 prediction that iron hydroxides sequestrate MB while precipitating.

#### 144 **Effect of various Fe<sup>0</sup> on the process of MB discoloration**

145 Figure 2 compares the extent of MB discoloration by tested Fe<sup>0</sup> materials in the presence and  
146 in the absence of MnO<sub>2</sub>. From Fig. 2a the following order of efficiency can be observed:  
147 ZVI3 < ZVI1  $\cong$  ZVI4 < ZVI2. This order of efficiency was the same than that obtained by  
148 Noubactep et al. [2] while testing the same materials for U<sup>VI</sup> removal and for Fe dissolution in  
149 0.02 M EDTA ( see also Tab. 2). These results suggest that MB discoloration in Fe<sup>0</sup>/H<sub>2</sub>O  
150 systems is a simple method to differentiate the reactivity of materials. However, due to the  
151 diversity of possible discoloration mechanisms, it was important to make sure that Fe<sup>0</sup>  
152 oxidative dissolution is evidenced. For this purpose MnO<sub>2</sub> is added to the systems to evidence  
153 the effects of in-situ generated Fe<sup>II</sup>. Fig. 2b summarises the results. The same order of  
154 reactivity was found (ZVI3 < ZVI1  $\cong$  ZVI4 < ZVI2). A close consideration of Fig. 2b reveals  
155 that ZVI3 is low reactive (assumption 1: *no delay of MB discoloration*) because unlike for the

156 three other materials no initial discoloration decrease was observed upon MnO<sub>2</sub> addition. All  
157 other materials are more reactive than ZVI3 (assumption 2: *the more extensive the*  
158 *discoloration delay the more reactive the sample*). Powdered ZVI2 was the most reactive  
159 material. The increased MB discoloration efficiency with ZVI2 is due to the increased Fe<sup>0</sup>  
160 surface area resulting in a better solid/H<sub>2</sub>O contact. Again granular ZVI1 and ZVI4 showed  
161 very close reactivity, suggesting that the MB discoloration method is as powerful as the two  
162 other tests but essentially simpler. The reactivity of used materials is also reflected by the  
163 final pH value (Eq. 2). According to Eq. 2 (H<sup>+</sup> production), the more reactive a material, the  
164 lower the final pH value (Tab. 2).



166 The verification of assumptions 1 and 2 validates the efficiency of MB discoloration for  
167 testing the reactivity of Fe<sup>0</sup> materials in Fe<sup>0</sup>/MnO<sub>2</sub>/H<sub>2</sub>O systems.

## 168 **Conclusions**

169 Methylene blue has been used for the characterization of the reactivity of Fe<sup>0</sup> materials. The  
170 proposed method is simple and does not involve any stringent reaction conditions. This  
171 method is a good alternative for reported costly instrumental procedures [2]. The proposed  
172 method has been successfully applied to differentiate the reactivity of four Fe<sup>0</sup> materials of  
173 known relative reactivity. This method can be used for material screening prior to cost-  
174 intensive investigations. Moreover, the test can be further developed to yield a characteristic  
175 parameter for Fe<sup>0</sup> materials similar to iodine number or methylene blue number for the  
176 characterization of activated carbons [16,18].

## 177 **Acknowledgments**

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246 decomposition of azo-dye water pollutants in weak acidic solutions. *Applied Catalysis*  
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- 248

248 **Table 1:** Main characteristics and iron content of the four tested Fe<sup>0</sup> materials. The material code  
 249 (“code”) are from the author, the given form is as supplied; d (μm) is the diameter of the supplied  
 250 material and the Fe content is given in % mass.

<b>Supplier<sup>(a)</sup></b>	<b>Supplier denotation</b>	<b>code</b>	<b>form</b>	<b>d</b> (μm)	<b>Fe</b> (%)
<b>MAZ, mbH</b>	Sorte 69 <sup>(b)</sup>	ZVI1	fillings	-	93 <sup>(c)</sup>
<b>G. Maier GmbH</b>	FG 0000/0080	ZVI2	powder	≤ 80	92 <sup>(d)</sup>
<b>Würth</b>	Hartgussstrahlmittel	ZVI3	spherical	1200	n.d. <sup>(e)</sup>
<b>ISPAT GmbH</b>	Schwammeisen	ZVI4	spherical	9000	n.d.

251 (a) List of suppliers: MAZ (Metallaufbereitung Zwickau, Co) in Freiberg (Germany); Gotthart Maier  
 252 Metallpulver GmbH (Rheinfelden, Germany), ISPAT GmbH, Hamburg (Germany), Connelly GPM Inc.  
 253 (USA), <sup>(b)</sup>Scrap iron material; <sup>(c)</sup>Mbudi et al. [19]; <sup>(d)</sup>average values from material supplier, <sup>(e)</sup>not  
 254 determined.

255

255 **Table 2:** Extent of MB discoloration ( $P_{MB}$ ) at a  $Fe^0$  mass loading of 9.0 g/L, decrease of the  
 256 percent MB discoloration ( $\Delta P_{MB}$ ), and final pH value in the presence of 5 g/L  $Fe^0$  as the  
 257  $MnO_2$  loading varied from 0 to 1.1 g/L. For ZVI3 no decrease ( $\Delta P_{MB} = 3.5\%$ ) was observed  
 258 under the experimental conditions ( $50\text{ min}^{-1}$  for 6 days). Data for the rate of iron dissolution  
 259 in a 2 mM EDTA solution ( $a_{EDTA}$ ) and the percent uranium removal ( $P_U$ ) are presented for  
 260 comparison.

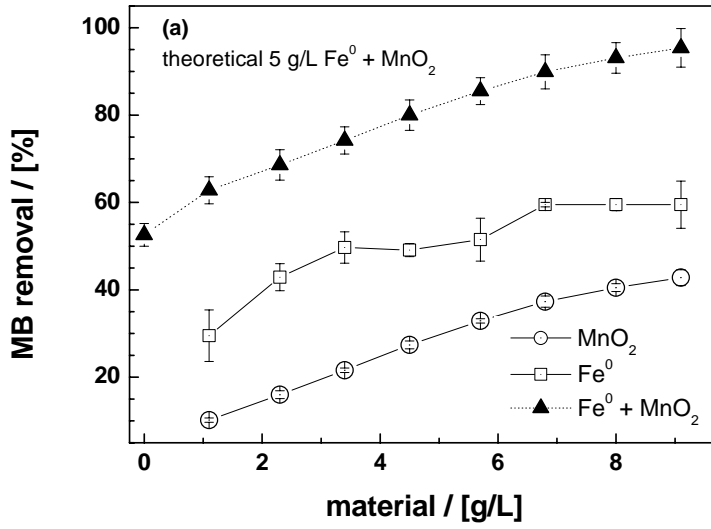
<b>Material</b>	<b><math>P_{MB}</math></b>	<b><math>\Delta P_{MB}</math></b>	<b><math>pH_{final}</math></b>	<b><math>a_{EDTA}^{(a)}</math></b>	<b><math>P_U^{(a)}</math></b>
	(%)	(%)		( $\mu\text{M/h}$ )	(%)
<b>ZVI1</b>	48.8	-4.8	7.8	1.95	81.0
<b>ZVI2</b>	100.0	-38.4	7.4	2.65	100.0
<b>ZVI3</b>	31.9	3.5	8.6	1.54	63.1
<b>ZVI4</b>	49.1	-8.7	7.9	1.86	87.0

261 <sup>(a)</sup> Values according to Noubactep et al. [2].

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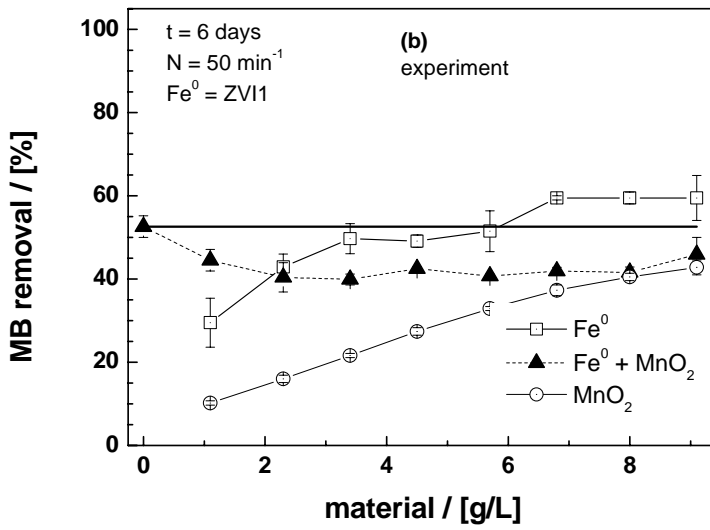
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Figure 1



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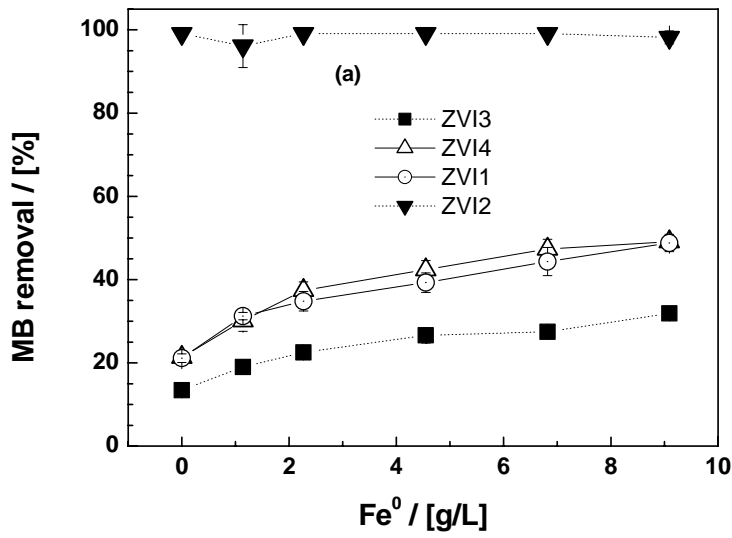
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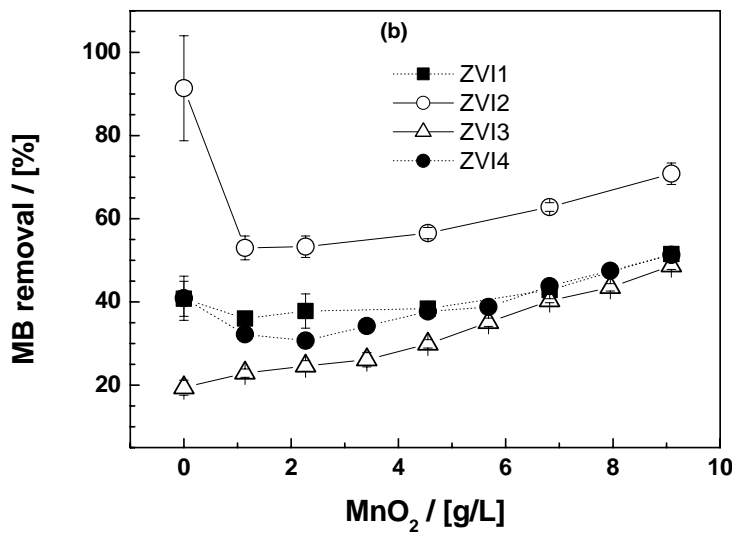
267 **Figure 2**

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278 **Figure Captions**

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280 **Figure 1:** Methylene blue discoloration by  $\text{MnO}_2$ ,  $\text{Fe}^0$ , and " $\text{Fe}^0 + \text{MnO}_2$ " for 6 days as a  
281 function of the material loading ( $\text{Fe}^0$ ,  $\text{MnO}_2$ ). ZVI1 is the used  $\text{Fe}^0$  source. In Fig  
282 1a the theoretical discoloration extent assuming additive removal of  $\text{Fe}^0$  (5 g/L)  
283 and varying amount of  $\text{MnO}_2$  is represented. Fig. 1b represents experimental  
284 results for the three systems together with the line corresponding to MB  
285 discoloration by 5 g/L  $\text{Fe}^0$  (no  $\text{MnO}_2$  addition). All lines are not fitting functions,  
286 they simply connect points to facilitate visualization.

287 **Figure 2:** Methylene blue discoloration by the individual  $\text{Fe}^0$  materials (a) and 5 g/L each  
288 material and varying amounts of  $\text{MnO}_2$  (b). The experiments were performed for 6  
289 days while shaking at  $50 \text{ min}^{-1}$ . The lines are not fitting functions, they simply  
290 connect points to facilitate visualization.